Document made available under the Patent Cooperation Treaty (PCT)

International application number: PCT/EP05/003045

International filing date: 21 March 2005 (21.03.2005)

Document type: Certified copy of priority document

Document details: Country/Office: EP

Number: 04101224.6

Filing date: 24 March 2004 (24.03.2004)

Date of receipt at the International Bureau: 12 May 2005 (12.05.2005)

Remark: Priority document submitted or transmitted to the International Bureau in

compliance with Rule 17.1(a) or (b)





Europäisches Patentamt

European Patent Office

Office européen des brevets

Bescheinigung

Certificate

Attestation

Die angehefteten Unterlagen stimmen mit der ursprünglich eingereichten Fassung der auf dem nächsten Blatt bezeichneten europäischen Patentanmeldung überein. The attached documents are exact copies of the European patent application described on the following page, as originally filed.

Les documents fixés à cette attestation sont conformes à la version initialement déposée de la demande de brevet européen spécifiée à la page suivante.

Patentanmeldung Nr. Patent application No. Demande de brevet nº

04101224.6

Der Präsident des Europäischen Patentamts; Im Auftrag

For the President of the European Patent Office

Le Président de l'Office européen des brevets p.o.

R C van Dijk

۶ ۶	
•	



Europäisches Patentamt

European Patent Office Office européen des brevets

PCT/EP2005/003045

Anmeldung Nr:

Application no.: 04101224.6

Demande no:

Anmeldetag:

Date of filing: 24.03.04

Date de dépôt:

Anmelder/Applicant(s)/Demandeur(s):

Basell Polyolefine GmbH Brühler Strasse 50389 Wesseling ALLEMAGNE

Bezeichnung der Erfindung/Title of the invention/Titre de l'invention: (Falls die Bezeichnung der Erfindung nicht angegeben ist, siehe Beschreibung. If no title is shown please refer to the description.
Si aucun titre n'est indiqué se referer à la description.)

Flexible propylene copolymer compositions having a high transparency

In Anspruch genommene Prioriät(en) / Priority(ies) claimed /Priorité(s) revendiquée(s)
Staat/Tag/Aktenzeichen/State/Date/File no./Pays/Date/Numéro de dépôt:

Internationale Patentklassifikation/International Patent Classification/Classification internationale des brevets:

C08L23/00

Am Anmeldetag benannte Vertragstaaten/Contracting states designated at date of filing/Etats contractants désignées lors du dépôt:

AT BE BG CH CY CZ DE DK EE ES FI FR GB GR HU IE IT LU MC NL PL PT RO SE SI SK TR LI

*		
•	-	
		j
		•
		•
		į.

Title

5

10

15

Flexible propylene copolymer compositions having a high transparency

The invention relates to propylene copolymer compositions, to a process for producing the propylene copolymer compositions, to the use of the propylene copolymer compositions of the present invention for producing fibers, films or moldings and also to fibers, films or moldings comprising the propylene copolymer compositions of the present invention.

Polymers of propylene can be processed to form shaped bodies which have advantageous mechanical properties, especially a high hardness, stiffness and shape stability. Consumer articles made of propylene polymers are used in a wide range of applications, e.g. as plastic containers, as household or office articles, toys or laboratory requisites. However, the products known from the prior art are not satisfactory for many applications, since a combination of low stiffness with good transparency is frequently desired.

It is known that multiphase propylene copolymers having a good impact toughness and a decreasing stiffness can be prepared by means of Ziegler-Natta catalyst systems in a multistage polymerization reaction. However, the incorporation of ethylene-propylene copolymers having a high proportion of ethylene into a polymer matrix makes the multiphase propylene copolymer turbid. Poor miscibility of the flexible phase with the polymer matrix leads to a separation of the phases and thus to turbidity and to poor transparency values of the heterogeneous copolymer. Furthermore, the ethylene-propylene rubber prepared by means of conventional Ziegler-Natta catalysts also has a very inhomogeneous composition.

It is also known that multiphase copolymers of propylene can be prepared using metallocene catalyst systems.

WO 94/28042 and EP-A 1 002 814 disclose multiphase copolymres of propylene. However, no propylene copolymer compositions having a propylene copolymer matrix are described.

WO 01/48034 relates to metallocene compounds by means of which propylene copolymers having a high molar mass and a high copolymerized ethylene content can be obtained under industrially relevant polymerization conditions. Multiphase propylene copolymers having a high stiffness/impact toughness level are obtainable in this way. However, no flexible propylene copolymer compositions having a high transparency are described.

WO 03/106523 relates to a flexible propylene composition obtained by a multistage process. However this document does not describes the particular balance of properties of the composition of the present invention, due to the particular values of comonomer content of

20

25

30

35

said composition, in particular this document does not describes an ethylene content lower than 1% in the propylene copolymer A).

It is an object of the present invention to overcome the above-described disadvantages of the prior art and to provide propylene copolymer compositions which have a well balanced properties of moldulus, melting point and at the same time a good transparency. Furthermore, they should have a low proportion of n-hexane-soluble material, a high impact toughness, in particular at low temperatures, good stress whitening behavior and a shrinkage behavior corresponding to propylene polymers.

We have found that this object is achieved by a propylene copolymer composition comprising:

- A) from 50% to 80% by weight of a propylene copolymer containing from 0.05 to 0.99% by weight of an alpha olefin having from 2 to 10 carbon atoms other than propylene; and
- B) from 20% to 50% by weight of one propylene copolymer containing from 7.01 to 9.99 % by weight of an alpha olefins having from 2 to 10 carbon atoms other than propylene;

said propylene copolymer composition having the following characteristics:

- (i) MFR (230°C/2,16 kg) comprised between 6 and 12 g/10min;
- (ii) Tensile E modulus comprised between 550 and 750 MPa (ISO 527-2:1993).

Preferably the propylene copolymer composition has the melting point, measured as described below, comprised between 143°C and 150°C; more preferably comprised between 145°C and 150°C.

Preferably the propylene copolymer composition has haze measured according to ASTM D 1003 comprised between 25% and 40%; preferably between 25% and 35%; more preferably between 31% and 35%, wherein the haze is measured on the product as such without the adding of clarifying agents.

The propylene copolymer composition object of the present invention is preferably obtainable by means of a two-stage or multistage polymerization using a catalyst system based on metallocene compounds.

In the multiphase propylene copolymer compositions of the present invention, the propylene copolymer A usually forms a three-dimensionally coherent phase in which the phase of the propylene copolymer B is embedded. Such a coherent phase in which one or more other

5

10

15

20

25

30

phases are dispersed is frequently referred to as the matrix. The matrix usually also makes up the major proportion by weight of the polymer composition.

In the multiphase propylene copolymer compositions of the present invention, the propylene copolymer B is generally dispersed in finely divided form in the matrix. Furthermore, the diameter of the then isolated domains of the propylene copolymer B is usually from 100 nm to 1000 nm. Preference is given to a geometry with a length in the range from 100 nm to 1000 nm and a thickness in the range from 100 to 300 nm. The determination of the geometry of the individual phases of the propylene copolymer compositions can be carried out, for example, by evaluation of contrasted transmission electron micrographs (TEMs).

To prepare the propylene polymers present in the propylene copolymer compositions of the present invention, at least one alpha olefin is used as monomer in addition to propylene. Preferred alpa-olefins are linear C_2 - C_{10} -1-alkenes. Particularly preferred olefins are ethylene and linear C_4 - C_{10} -1-alkenes such as 1-butene, 1-pentene, 1-hexene, 1-heptene, 1-octene, 1-decene, in particular ethylene and/or 1-butene.

The propylene copolymer A present in the propylene copolymer compositions of the present invention is a propylene copolymer containing from 0.05 to 0.99% by weight of alpha-olefins other than propylene. Preferred propylene copolymers contain from 0.5 to 0.90% by weight, in particular from 0.5 to 0.8% by weight, of alpha-olefins other than propylene. As comonomers, preference is given to using ethylene or linear C₄-C₁₀- 1-alkenes or mixtures thereof, in particular ethylene and/or 1-butene.

The component B present in the propylene copolymer compositions of the present invention is made up of at least one propylene copolymer containing from 7.01 to 9.99% by weight of alpha-olefins other than propylene. Preferred comonomers are ethylene or linear C_4 - C_{10} -1-alkenes or mixtures thereof, in particular ethylene and/or 1-butene. In a further, preferred embodiment, monomers containing at least two double bonds, e.g. 1,7-octadiene or 1,9-decadiene, are additionally used. The content of the alpha-olefins other than propylene in the propylene copolymers is preferably from 8 to 9.6 % by weight,

The composition object of the present invention contains from 50% to 80% by weight of the copolymer A; preferably from 60% to 75% by weight; more preferably from 65% to 72% by weight. The composition object of the present invention contains from 20% to 50% by weight of the propylene copolymer B; preferably from 25% to 40% by weight; more preferably from 28% to 35% by weight.

5

10

15

20

25

30

The proportion of n-hexane-soluble material in the propylene copolymer compositions of the present invention is preferably $\leq 2.6\%$ by weight, particularly preferably ≤ 2.0 by weight and in particular $\leq 1.0\%$ by weight. According to the present invention, the determination of the proportion of n-hexane-soluble material is carried out by a modified FDA method by extraction of about 2.5 g of material with one liter of n-hexane at 50°C. According to the FDA method, an extruded film is used as sample. However, in the case of the propylene copolymer compositions of the present invention, the same values for the proportion of n-hexane-soluble material are obtained using samples composed of granulated material or a granulated material which has been milled to a mean particle diameter of, for example, 100 μ m.

5

10

15

20

25

30

35

40

Furthermore, the propylene copolymer compositions of the present invention preferably have a haze value comprised between 25% and 40%, preferably between 25% and 35%; more preferably between 31% and 35%, based on a film thickness of the propylene copolymer composition of 1 mm. The haze value is a measure of the turbidity of the material and is thus a parameter which characterizes the transparency of the propylene copolymer compositions. The lower the haze value, the higher the transparency. Furthermore, the haze value is also dependent on the film thickness. The thinner the layer, the lower the haze value. The haze value is generally measured in accordance with the standard ASTM D 1003, with different test specimens being able to be used. According to the present invention, the propylene copolymer compositions are characterized by means of the haze value of injection-molded test specimens having a thickness of 1mm. The haze is measured on the polymer composition as such without the adding of clarifying agents, this means that lower values can be obtained simply by adding clarifying agents known in the art such as sodium benzoate, aluminum tertbutylbenzoate, dibenzylidenesorbitol or its C₁-C₈-alkyl-substituted derivatives such as methyldibenzylidenesorbitol, 3,4-dimethylbenzylidensorbitol, ethyldibenzylidenesorbitol or dimethyldibenzylidenesorbitol or salts of diesters of phosphoric acid, e.g. sodium 2,2'methylenebis(4,6,-di-tert-butylphenyl)phosphate.

Preferred propylene copolymer compositions of the present invention have a tensile E modulus determined in a tensile test in accordance with ISO 527-2:1993 in the range from 550 MPa to 700 MPa and in particular in the range from 600 MPa to 700 MPa.

Propylene polymers are tough materials at room temperature, i.e. plastic deformation occurs under mechanical stress only before the material breaks. However, at reduced temperatures, propylene polymers display brittle fracture, i.e. fracture occurs virtually without deformation or at a high propagation rate. A parameter which describes the temperature at which the

deformation behavior changes from tough to brittle is the "brittle/tough transition temperature".

5

10

15

20

25

30

35

40

In the propylene copolymer compositions of the present invention, the propylene copolymer A is generally present as matrix and the propylene copolymer B, which usually has a stiffness lower than that of the matrix and acts as impact modifier, is dispersed therein in finely divided form. Such an impact modifier not only increases the toughness at elevated temperatures but also reduces the brittle/tough transition temperature. For the purposes of the present invention, the brittle/tough transition temperature is determined by means of puncture tests in accordance with ISO 6603-2, in which the temperature is reduced in continuous steps. The force/displacement graphs recorded in the puncture tests enable conclusions as to the deformation behavior of the test specimens at the respective temperature to be drawn and thus allow the brittle/tough transition temperature to be determined. To characterize the specimens according to the present invention, the temperature is reduced in steps of 2°C and the brittle/tough transition temperature is defined as the temperature at which the total deformation is at least 25% below the mean total deformation of the preceding 5 measurements; here, the total deformation is the displacement through which the punch has traveled when the force has passed through a maximum and dropped to 3% of this maximum force. In the case of specimens which do not display a sharp transition and in which none of the measurements meet the specified criterion, the total deformation at 23°C is employed as reference value and the brittle/tough transition temperature is the temperature at which the total deformation is at least 25% below the total deformation at 23°C. Preferred propylene copolymer compositions of the present invention have a brittle/tough transition temperature comprised between -20°C and 0°C, preferably comprised between -15°C and -3 °C and more preferably comprised between -10°C and -5°C.

Furthermore, the propylene copolymer compositions of the present invention usually display good stress whitening behavior. For the purposes of the present invention, stress whitening is the occurrence of whitish discoloration in the stressed region when the polymer is subjected to mechanical stress. In general, it is assumed that the white discoloration is caused by small voids being formed in the polymer under mechanical stress. Good stress whitening behavior means that no or only very few regions having a whitish discoloration occur under mechanical stress.

One method of quantifying stress whitening behavior is to subject defined test specimens to a defined impact stress and then to measure the size of the resulting white spots. Accordingly,

in the dome method, a falling dart is dropped onto a test specimen in a falling dart apparatus in accordance with DIN 53443 Part 1. In this method, a falling dart having a mass of 250 g and a punch of 5 mm in diameter is used. The dome radius is 25 mm and the drop is 50 cm. The test specimens used are injection-molded circular disks having a diameter of 60 mm and a thickness of 2 mm, and each test specimen is subjected to only one impact test. The stress whitening is reported as the diameter of the visible stress whitening region in mm; the value reported is in each case the mean of 5 test specimens and the individual values are determined as the mean of the two values in the flow direction on injection molding and perpendicular thereto on the side of the circular disk opposite that on which impact occurs.

5

10

15

20

40

The propylene copolymer compositions of the present invention generally display no or only very little stress whitening determined by the dome method at 23°C. In the case of preferred propylene copolymer compositions, a value of from 0 to 8 mm, preferably from 0 to 5 mm and in particular from 0 to 2.5 mm, is determined by the dome method at 23°C. Very particularly preferred propylene copolymer compositions display no stress whitening at all in the test carried out by the dome method at 23°C.

The propylene copolymer compositions of the present invention generally further comprise customary amounts of customary additives known to those skilled in the art, e.g. stabilizers, lubricants and mold release agents, fillers, nucleating agents, antistatics, plasticizers, dyes, pigments or flame retardants. In general, these are incorporated during granulation of the pulverulent product obtained in the polymerization.

Customary stabilizers include antioxidants such as sterically hindered phenols, processing stabilizers such as phosphites or phosphonites, acid scavengers such as calcium stearate or zinc stearate or dihydrotalcite, sterically hindered amines or UV stabilizers. In general, the propylene copolymer compositions of the present invention contain one or more stabilizers in amounts of up to 2% by weight.

Suitable lubricants and mold release agents are, for example, fatty acids, calcium or zinc salts of fatty acids, fatty acid amides or low molecular weight polyolefin waxes, which are usually used in concentrations of up to 2% by weight.

Possible fillers are, for example, talc, chalk or glass fibers, and these are usually used in amounts of up to 50% by weight.

Examples of suitable nucleating agents are inorganic additives such as talc, silica or kaolin, salts of monocarboxylic or polycarboxylic acids, e.g. sodium benzoate or aluminum tert-butylbenzoate, dibenzylidenesorbitol or its C_1 - C_8 -alkyl-substituted derivatives such as

methyldibenzylidenesorbitol, ethyldibenzylidenesorbitol or dimethyldibenzylidenesorbitol or salts of diesters of phosphoric acid, e.g. sodium 2,2'-methylenebis(4,6,-di-tert-butylphenyl)phosphate. The nucleating agent content of the propylene copolymer composition is generally up to 5% by weight.

Such additives are generally commercially available and are described, for example, in Gächter/Müller, Plastics Additives Handbook, 4th Edition, Hansa Publishers, Munich, 1993.

5

10

15

20

25

30

35

40

In a preferred embodiment, the propylene copolymer compositions of the present invention contain from 0.1 to 1% by weight, preferably from 0.15 to 0.25% by weight, of a nucleating agent, in particular dibenzylidenesorbitol or a dibenzylidenesorbitol derivative, particularly preferably dimethyldibenzylidenesorbitol.

In the case of preferred propylene copolymer compositions obtained from propylene and ethylene, the structure of the propylene-ethylene copolymers B can be determined by means of 13 C-NMR spectroscopy as well as by means IR spectroscopy. Evaluation of the spectrum is prior art and can be carried out by a person skilled in the art using, for example, the method described by H. N. Cheng, Macromolecules 17 (1984), pp. 1950-1955 or L. Abis et al., Makromol. Chemie 187 (1986), pp. 1877-1886. The structure can then be described by the proportions of "PE_x" and of "PEP", where PE_x refers to the propylene-ethylene units having \geq 2 successive ethylene units and PEP refers to the propylene-ethylene units having an isolated ethylene unit between two propylene units. Preferred propylene copolymer compositions obtained from propylene and ethylene have a PEP/PE_x ratio in the range from 0.9 to 2.2, preferably in the range from 1 to 2.0, particularly preferably in the range from 1.3-2.0.

The properties of the propylene copolymer compositions of the present invention are also determined by the viscosity ratio of the propylene copolymer B and the propylene copolymer A, i.e. the ratio of the molar mass of the dispersed phase to the molar mass of the matrix. In particular, this influences the transparency.

To determine the viscosity ratio, the propylene copolymer compositions can be fractionated by means of TREF fractionation (Temperature Rising Elution Fractionation). The propylene copolymer B is then the combined fractions which are eluted by xylene at temperatures up to and including 70°C. The propylene copolymer A is obtained from the combined fractions which are eluted by xylene at temperatures above 70°C. However, at high comonomer contents in the propylene comonomers A, a clean TREF fractionation presents difficulties since the elution temperature of the propylene copolymer A drops below 70°C with increasing comonomer content. One way of obtaining information about the individual components is to

carry out the examination of the propylene copolymer A using the polymer taken from the reactor directly after the first polymerization step. The propylene copolymer B can be separated from the product of a separate test run in which a polymerization identical to that for the propylene copolymer composition to be examined has been carried out but with no addition of comonomer in the first polymerization step, i.e. a propylene homopolymer has been prepared. The shear viscosity of the polymers is determined on the components obtained in this way. The determination is usually carried out by a method based on ISO 6721-10 using a rotation viscometer having a plate/plate geometry, diameter = 25 mm, amplitude = 0.05-0.5, preheating time = 10-12 min, at a temperature of from 200 to 230°C. The ratio of the shear viscosity of propylene copolymer B to that of propylene copolymer A is then reported at a shear rate of $100s^{-1}$.

5

10

15

20

25

30

35

40

In preferred propylene copolymer compositions, the ratio of the shear viscosity of propylene copolymer B to that of propylene copolymer A at a shear rate of $100s^{-1}$ is in the range from 0.3 to 2.5, preferably from 0.5 to 2 and particularly preferably in the range from 0.7 to 1.75.

The propylene copolymer compositions of the present invention preferably have a narrow molar mass distribution M_w/M_n . The molar mass distribution M_w/M_n is, for the purposes of the invention, the ratio of the weight average molar mass M_w to the number average molar mass M_n . The molar mass distribution M_w/M_n is preferably in the range from 1.5 to 3.5, particularly preferably in the range from 2 to 2.5 and in particular in the range from 2 to 2.4.

The molar mass M_n of the propylene copolymer compositions of the present invention is preferably in the range from 20,000 g/mol to 500,000 g/mol, particularly preferably in the range from 50,000 g/mol to 200,000 g/mol and very particularly preferably in the range from 80,000 g/mol to 150,000 g/mol.

The composition of the present invention is preferably carried out in a multistage polymerization process comprising at least two successive polymerization steps which are generally carried out in a reactor cascade. It is possible to use the customary reactors employed for the preparation of propylene polymers.

The polymerization can be carried out in a known manner in bulk, in suspension, in the gas phase or in a supercritical medium. It can be carried out batchwise or preferably continuously. Solution processes, suspension processes, stirred gas-phase processes or gas-phase fluidized-bed processes are possible. As solvents or suspension media, it is possible to use inert hydrocarbons, for example isobutane, or else the monomers themselves. It is also possible to carry out one or more steps of the process of the present invention in two or more reactors.

The size of the reactors is not of critical importance for the process of the present invention. It depends on the output which is to be achieved in the individual reaction zone(s).

Preference is given to processes in which the polymerization in the second step in which the propylene copolymer(s) B is/are formed takes place from the gas phase. The preceding polymerization of the propylene copolymers A can be carried out either in block, i.e. in liquid propylene as suspension medium, or else from the gas phase. If all polymerizations take place from the gas phase, they are preferably carried out in a cascade comprising stirred gas-phase reactors which are connected in series and in which the pulverulent reaction bed is kept in motion by means of a vertical stirrer. The reaction bed generally consists of the polymer which is polymerized in the respective reactor. If the initial polymerization of the propylene copolymers A is carried out in bulk, preference is given to using a cascade made up of one or more loop reactors and one or more gas-phase fluidized-bed reactors. The preparation can also be carried out in a multizone reactor.

To prepare the propylene copolymers present in the propylene copolymer compositions of the present invention, preference is given to using catalyst systems based on metallocene compounds of transition metals of group 3, 4, 5 or 6 of the Periodic Table of the Elements.

Particular preference is given to catalyst systems based on metallocene compounds of the formula (I),

25

30

5

10

15

20

35

where

M is zirconium, hafnium or titanium, preferably zirconium,

X are identical or different and are each, independently of one another, hydrogen or halogen or an -R, -OR, -OSO₂CF₃, -OCOR, -SR, -NR₂ or -PR₂ group, where R is

linear or branched C₁-C₂₀-alkyl, C₃-C₂₀-cycloalkyl which may be substituted by one or more C₁-C₁₀-alkyl radicals, C₆-C₂₀-aryl, C₇-C₂₀-alkylaryl or C₇-C₂₀-arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the Elements or one or more unsaturated bonds, preferably C₁-C₁₀-alkyl such as methyl, ethyl, n-propyl, isopropyl, n-butyl, isobutyl, sec-butyl, tert-butyl, n-pentyl, n-hexyl, n-heptyl or n-octyl or C_3 - C_{20} -cycloalkyl such as cyclopentyl or cyclohexyl, where the two radicals X may also be joined to one another and preferably form a C₄-C₄₀dienyl ligand, in particular a 1,3-dienyl ligand, or an -OR'O- group in which the R' substituent is divalent group selected from the group consisting of C₁-C₄₀-alkylidene, C₆-C₄₀-arylidene, C₇-C₄₀alkylarylidene C₇-C₄₀-arylalkylidene, and where X is preferably a halogen atom or an -R or -OR group or the two radicals X form an -OR'O- group and X is particularly preferably chlorine or methyl,

is a divalent bridging group selected from the group consisting of C_1 - C_{20} -alkylidene radicals, C_3 - C_{20} -cycloalkylidene radicals, C_6 - C_{20} -arylidene radicals, C_7 - C_{20} -alkylarylidene radicals and C_7 - C_{20} -arylalkylidene radicals, which may contain heteroatoms of groups 13-17 of the Periodic Table of the Elements, or a silylidene group having up to 5 silicon atoms, e.g. $-SiMe_2$ — or $-SiPh_2$ —, where L preferably is a radical selected from the group consisting of $-SiMe_2$ —, $-SiPh_2$ —,

-SiPhMe-, -SiMe(SiMe₃)-, -CH₂-, -(CH₂)₂-, -(CH₂)₃- and -C(CH₃)₂-,

is linear or branched C_1 - C_{20} -alkyl, C_3 - C_{20} -cycloalkyl which may be substituted by one or more C_1 - C_{10} -alkyl radicals, C_6 - C_{20} -aryl, C_7 - C_{20} -alkylaryl or C_7 - C_{20} -arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the Elements or one or more unsaturated bonds, where R^1 is preferably unbranched in the α position and is preferably a linear or branched C_1 - C_{10} -alkyl group which is unbranched in the α position, in particular a linear C_1 - C_4 -alkyl group such as methyl, ethyl, n-propyl or n-butyl,

35 R^2 is a group of the formula $-C(R^3)_2R^4$, where

5

10

15

20

25

30

40

 \mathbb{R}^1

 \mathbb{R}^3

L

are identical or different and are each, independently of one another, linear or branched C_1 - C_{20} -alkyl, C_3 - C_{20} -cycloalkyl which may be substituted by one or more C_1 - C_{10} -alkyl radicals, C_6 - C_{20} -aryl, C_7 - C_{20} -alkylaryl or C_7 - C_{20} -arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the

Elements or one or more unsaturated bonds, or two radicals R^3 may be joined to form a saturated or unsaturated C_3 - C_{20} -ring,

where R3 is preferably a linear or branched C1-C10-alkyl group, and

 R^4 is hydrogen or linear or branched C_1 - C_{20} -alkyl, C_3 - C_{20} -cycloalkyl which may be substituted by one or more C_1 - C_{10} -alkyl radicals, C_6 - C_{20} -aryl, C_7 - C_{20} -alkylaryl or C_7 - C_{20} -arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic

Table of the Elements or one or more unsaturated bonds, where R⁴ is preferably hydrogen,

T and T' are divalent groups of the formulae (II), (III), (IV), (V) or (VI),

where

 \mathbb{R}^5

25

30

35

5

10

the atoms denoted by the symbols * and ** are joined to the atoms of the compound of the formula (I) which are denoted by the same symbol, and

are identical or different and are each, independently of one another, hydrogen or halogen or linear or branched C₁-C₂₀-alkyl, C₃-C₂₀-cycloalkyl which may be substituted by one or more C₁-C₁₀-alkyl radicals, C₆-C₂₀-aryl, C₇-C₂₀-alkylaryl or C₇-C₂₀-arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the Elements or one or more unsaturated bonds, where R⁵ is preferably hydrogen or a linear or branched C₁-C₁₀-alkyl group, in particular a linear C₁-C₄-alkyl group such as methyl, ethyl, n-propyl or n-butyl, and are identical or different and are each, independently of one another, halogen or linear or branched C₁-C₂₀-alkyl, C₃-C₂₀-cycloalkyl which may be substituted by one

R⁶

or more C_1 - C_{10} -alkyl radicals, C_6 - C_{20} -aryl, C_7 - C_{20} -alkylaryl or C_7 - C_{20} -arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the Elements or one or more unsaturated bonds, where R^6 is preferably an aryl group of the formula (VII),

$$R^7$$
 R^7
 R^8
(VII)

where

 \mathbb{R}^{8}

25

30

35

5

10

15 \mathbb{R}^7 are identical or different and are each, independently of one another, hydrogen or halogen or linear or branched C₁-C₂₀-alkyl, C₃-C₂₀-cycloalkyl which may be substituted by one or more C₁-C₁₀-alkyl radicals, C₆-C₂₀-aryl, C₇-C₂₀-alkylaryl or C₇-C₂₀-arylalkyl and may contain one or more heteroatoms of groups 13-17 of the 20 Periodic Table of the Elements or one or more unsaturated bonds, or two radicals R⁷ mav be joined to form a saturated or unsaturated C_3-C_{20} ring, where R⁷ is preferably a hydrogen atom, and

is hydrogen or halogen or linear or branched C_1 - C_{20} -alkyl, C_3 - C_{20} -cycloalkyl which may be substituted by one or more C_1 - C_{10} -alkyl radicals, C_6 - C_{20} -aryl, C_7 - C_{20} -alkylaryl or C_7 - C_{20} -arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the Elements or one or more unsaturated bonds, where R^8 is preferably a branched alkyl group of the formula $-C(R^9)_3$, where

R⁹ are identical or different and are each, independently of one another, a linear or branched C₁-C₆-alkyl group or two or three of the radicals R⁹ are joined to form one or more ring systems.

It is preferred that at least one of the groups T and T' is substituted by a radical R⁶ of the formula (VII); it is particularly preferred that both groups are substituted by such a radical. Very particular preference is given to at least one of the groups T and T' being a group of the formula (IV) which is substituted by a radical R⁶ of the formula (VII) and the other either has the formula (II) or (IV) and is likewise substituted by a radical R⁶ of the formula (VII).

The greatest preference is given to catalyst systems based on metallocene compounds of the formula (VIII),

5

$$R^{1}$$
 R^{5}
 R^{5}

15

10

25

Particularly useful metallocene compounds and methods of preparing them are described, for example, in WO 01/48034 and the European patent application No. 01204624.9.

It is also possible to use mixtures of various metallocene compounds or mixtures of various catalyst systems. However, preference is given to using only one catalyst system comprising one metallocene compound, which is used for the polymerization of the propylene copolymer A and the propylene copolymer B.

Examples of useful metallocene compounds are

dimethylsilanediyl(2-ethyl-4-(4'-tert-butylphenyl)indenyl)(2-isopropyl-4-(4'-tert-butylphenyl)indenyl)

30 butylphenyl)indenyl)zirconium dichloride,

dimethylsilanediyl(2-methyl-4-(4'-tert-butylphenyl)indenyl)(2-isopropyl-4-(1-naphthyl)indenyl)zirconium dichloride,

dimethylsilanediyl(2-methyl-4-phenyl-1-indenyl)(2-isopropyl-4-(4'-tert-butylphenyl)-1-

indenyl)zirconium dichloride,

dimethylsilanediyl(2-methylthiapentenyl)(2-isopropyl-4-(4'-tert-butylphenyl)indenyl)-

zirconium

dichloride,

40

dimethylsilanediyl(2-isopropyl-4-(4'-tert-butylphenyl)indenyl)(2-methyl-4,5-benzindenyl)-zirconium dichloride,

dimethylsilanediyl(2-methyl-4-(4'-tert-butylphenyl)indenyl)(2-isopropyl-4-(4'-tert-butylphenyl)indenyl)

butylphenyl)indenyl)zirconium dichloride,

dimethylsilanediyl(2-methyl-4-(4'-tert-butylphenyl)indenyl)(2-isopropyl-4-phenylindenyl)-zirconium dichloride,

dimethylsilanediyl(2-ethyl-4-(4'-tert-butylphenyl)indenyl)(2-isopropyl-4-phenyl)indenyl)-zirconium dichloride and

dimethylsilanediyl(2-isopropyl-4-(4'-tert-butylphenyl)indenyl)(2-methyl-4-(1-naphthyl)indenyl)zirconium dichloride

and mixtures thereof.

5

10

15

20

25

30

The preferred catalyst systems based on metallocene compounds generally further comprise cation-forming compounds as cocatalysts. Suitable cation-forming compounds which are able to react with the metallocene compound to convert it into a cationic compound are, for example, compounds such as an aluminoxane, a strong uncharged Lewis acid, an ionic compound having a Lewis-acid cation or an ionic compound containing a Brönsted acid as cation. The cation-forming compounds are frequently also referred to as compounds which form metallocenium ions.

As aluminoxanes, it is possible to use, for example, the compounds described in WO 00/31090. Particularly useful compounds are open-chain or cyclic aluminoxane compounds of the formula (IX) or (X)

 $\begin{array}{c|c}
\hline
 O & AI & m \\
\hline
 R^{21}
\end{array}$

where

5

10

15

25

30

35

 R^{21} is a C_1 - C_4 -alkyl group, preferably a methyl or ethyl group, and

m is an integer from 5 to 30, preferably from 10 to 25.

These oligomeric aluminoxane compounds are usually prepared by reacting a solution of trialkylaluminum with water. The oligomeric aluminoxane compounds obtained in this way are generally in the form of mixtures of both linear and cyclic chain molecules of various lengths, so that m is to be regarded as a mean. The aluminoxane compounds can also be present in admixture with other metal alkyls, preferably aluminum alkyls.

Furthermore, modified aluminoxanes in which some of the hydrocarbon radicals or hydrogen atoms are replaced by alkoxy, aryloxy, siloxy or amide radicals may be used in place of the aluminoxane compounds of the formulae (IX) or (X).

It has been found to be advantageous to use the metallocene compounds and the aluminoxane compounds in such amounts that the atomic ratio of aluminum from the aluminoxane compounds to the transition metal from the metallocene compound is in the range from 10:1 to 1000:1, preferably from 20:1 to 500:1 and in particular in the range from 30:1 to 400:1.

As strong, uncharged Lewis acids, preference is given to compounds of the formula (XI)

 $M^2X^1X^2X^3$ (XI)

where

M² is an element of group 13 of the Periodic Table of the Elements, in particular B, Al or G and preferably B,

 X^1 , X^2 and X^3 are each hydrogen, C_1 – C_{10} –alkyl, C_6 – C_{15} –aryl, alkylaryl, arylalkyl, haloalkyl or haloaryl each having from 1 to 10 carbon atoms in the alkyl radical and from 6 to 20 carbon atoms in the aryl radical, or fluorine, chlorine, bromine or iodine, in particular a haloaryl, preferably pentafluorophenyl.

Further examples of strong, uncharged Lewis acids are mentioned in WO 00/31090.

Particular preference is given to compounds of the formula (XI) in which X^1 , X^2 and X^3 are identical, preferably tris(pentafluorophenyl)borane.

Strong uncharged Lewis acids suitable as cation-forming compounds also include the reaction products from the reaction of a boronic acid with two equivalents of a trialkylaluminum or the reaction products from the reaction of a trialkylaluminum with two equivalents of an acidic

fluorinated, in particular perfluorinated, carbon compound such as pentafluorophenol or bis(pentafluorophenyl) borinic acid.

Suitable ionic compounds containing Lewis-acid cations include salt-like compounds of the cation of the formula (XII)

$$[(Y^{a+})Q_1Q_2...Q_z]^{d+}$$
 (XII)

where

5

10

15

20

25

30

35

Y is an element of groups 1 to 16 of the Periodic Table of the Elements,

 Q_1 to Q_z are singly negatively charged groups such as C_1 – C_{28} –alkyl, C_6 – C_{15} –aryl, alkylaryl, arylalkyl, haloalkyl, haloaryl each having from 6 to 20 carbon atoms in the aryl radical and from 1 to 28 carbon atoms in the alkyl radical, C_3 – C_{10} –cycloalkyl which may be substituted by C_1 – C_{10} –alkyl groups, or halogen, C_1 – C_{28} –alkoxy, C_6 – C_{15} –aryloxy, silyl or mercapto groups,

a is an integer from 1 to 6 and

z is an integer from 0 to 5,

d is the difference a-z, but d is greater than or equal to 1.

Particularly useful Lewis-acid cations are carbonium cations, oxonium cations and sulfonium cations and also cationic transition metal complexes. Particular mention may be made of the triphenylmethyl cation, the silver cation and the 1,1'-dimethylferrocenyl cation. They preferably have noncoordinating counterions, in particular boron compounds as are mentioned in WO 91/09882, preferably tetrakis(pentafluorophenyl)borate.

Salts having noncoordinating anions can also be prepared by combining a boron or aluminum compound, e.g. an aluminum alkyl, with a second compound which can react to link two or more boron or aluminum atoms, e.g. water, and a third compound which forms an ionizing ionic compound with the boron or aluminum compound, e.g. triphenylchloromethane. A fourth compound which likewise reacts with the boron or aluminum compound, e.g. pentafluorophenol, can additionally be added.

Ionic compounds containing Brönsted acids as cations preferably likewise have noncoordinating counterions. As Brönsted acids, particular preference is given to protonated amine or aniline derivatives. Preferred cations are N,N-dimethylanilinium, N,N-dimethylcylohexylammonium and N,N-dimethylbenzylammonium and also derivatives of the latter two.

Preferred ionic compounds C) are, in particular, N,N-dimethylanilinium tetrakis(pentafluorophenyl)borate, N,N-dimethylcyclohexylammonium tetrakis(pentafluorophenyl)borate and N,N-dimethylbenzylammonium tetrakis(pentafluorophenyl)borate.

It is also possible for two or more borate anions to be joined to one another, as in the dianion $[(C_6F_5)_2B-C_6F_4-B(C_6F_5)_2]^2$, or the borate anion can be bound via a bridge having a suitable functional group to the support surface.

Further suitable cation-forming compounds are listed in WO 00/31090.

The amount of strong, uncharged Lewis acids, ionic compounds having Lewis-acid cations or ionic compounds containing Brönsted acids as cations is preferably from 0.1 to 20 equivalents, preferably from 1 to 10 equivalents, based on the metallocene compound.

Suitable cation-forming compounds also include boron-aluminum compounds such as di[bis(pentafluorophenylboroxy)]methylalane. Such boron-aluminum compounds are disclosed, for example, in WO 99/06414.

It is also possible to use mixtures of all of the abovementioned cation-forming compounds. Preferred mixtures comprise aluminoxanes, in particular methylaluminoxane, and an ionic compound, in particular one containing the tetrakis(pentafluorophenyl)borate anion, and/or a strong

uncharged Lewis acid, in particular tris(pentafluorophenyl)borane.

Preference is given to using both the metallocene compound and the cation-forming compound in a solvent, preferably aromatic hydrocarbons having from 6 to 20 carbon atoms, in

xylenes and toluene.

The preferred catalyst systems based on metallocene compounds can further comprise, as additional component, a metal compound of the formula (XIII),

 $M^3 (R^{22})_r (R^{23})_s (R^{24})_t$ (XIII)

where

M³ is an alkali metal, an alkaline earth metal or a metal of group 13 of the Periodic Table, i.e. boron, aluminum, gallium, indium or thallium,

is hydrogen, C_1 – C_{10} –alkyl, C_6 – C_{15} –aryl, alkylaryl or arylalkyl each having from 1 to 10 carbon atoms in the alkyl part and from 6 to 20 carbon atoms in the aryl part,

15

20

25

 R^{23} and R^{24} are each hydrogen, halogen, C_1 – C_{10} –alkyl, C_6 – C_{15} –aryl, alkylaryl, arylalkyl or alkoxy each having from 1 to 10 carbon atoms in the alkyl radical and from 6 to 20 carbon atoms in the aryl radical,

is an integer from 1 to 3

and

r

5

10

15

25

30

35

s and t are integers from 0 to 2, where the sum r+s+t corresponds to the valence of M³, where the metal compound of the formula (XIII) is not identical to the cation-forming compound. It is also possible to use mixtures of various metal compounds of the formula (XIII).

Among metal compounds of the formula (XIII), preference is given to those in which M³ is lithium, magnesium or aluminum and

 R^{23} and R^{24} are each C_1 – C_{10} –alkyl.

Particularly preferred metal compounds of the formula (XIII) are n-butyllithium, n-butyl-n-octylmagnesium, n-butyl-n-heptylmagnesium, tri-n-hexylaluminum, triisobutylaluminum, triethyl-aluminum and trimethylaluminum and mixtures thereof.

If a metal compound of the formula (XIII) is used, it is preferably used in such an amount that
the molar ratio of M³ from formula (XIII) to the transition metal from the metallocene compound is from 800:1 to 1:1, in particular from 200:1 to 2:1.

The preferred catalyst systems based on metallocene compounds are usually used in supported form. Suitable supports are, for example, porous organic or inorganic inert solids such as finely divided polymer powders, talc, sheet silicates or inorganic oxides. Inorganic oxides suitable as supports may be found among the oxides of elements of groups 2, 3, 4, 5, 13, 14, 15 and 16 of the Periodic Table of the Elements. Preference is given to oxides or mixed oxides of the elements calcium, aluminum, silicon, magnesium or titanium and also corresponding oxide mixtures. Other inorganic oxides which can be used alone or in combination with the abovementioned oxidic supports are, for example, ZrO₂ or B₂O₃. Preferred oxides are silicon dioxide and aluminum oxide, in particular silica gels or pyrogenic of silicas. An example preferred mixed oxide calcined a is hydrotalcite.

The support materials used preferably have a specific surface area in the range from 10 to 1000 m²/g, preferably from 50 to 500 m²/g and in particular from 200 to 400 m²/g, and a pore volume in the range from 0.1 to 5 ml/g, preferably from 0.5 to 3.5 ml/g and in particular from

0.8 to 3.0 ml/g. The mean particle size of the finely divided supports is generally in the range from 1 to 500 m, preferably from 5 to 350 m and in particular from 10 to 100 m.

In the preparation of the propylene copolymers present in the propylene copolymer compositions of the present invention, preference is given to firstly forming the propylene copolymer A in a first step by polymerizing from 80% by weight to 99% by weight, based on the total weight of the mixture, of propylene in the presence of further olefins, usually at from 40°C to 120°C and pressures in the range from 0.5 bar to 200 bar. The polymer obtainable by means of this reaction subsequently has a mixture of from 2 to 95% by weight of propylene and from 5% to 98% by weight of further olefins polymerized onto it in a second step, usually at from 40°C to 120°C and pressures in the range from 0.5 bar to 200 bar. The polymerization of the propylene copolymer A is preferably carried out at from 60 to 80°C, particularly preferably from 10 bar to 50 bar. The polymerization of the propylene copolymer B is preferably carried out at from 60 to 80°C, particularly preferably from 5 to 100 bar, particularly preferably from 5 to 100 bar, particularly preferably from 5 to 100 bar, particularly preferably from 10 bar to 50 bar.

In the polymerization, it is possible to use customary additives, for example molar mass regulators such as hydrogen or inert gases such as nitrogen or argon.

The amounts of the monomers added in the individual steps and also the process conditions such as pressure, temperature or the addition of molar mass regulators such as hydrogen is chosen so that the polymers formed have the desired properties. The scope of the invention includes the technical teaching that a propylene copolymer composition which has a low stiffness and at the same time a good transparency is obtainable, for example, by setting defined comonomer contents of the propylene copolymers A and B and the viscosity ratio of propylene copolymer A to propylene copolymer B.

The composition of the propylene copolymer B has significant effects on the transparency of the propylene copolymer compositions of the present invention. A reduction in the comonomer content of the propylene copolymer B leads to an improved transparency, while at the same time the stiffness of the matrix also decreases as a result of the better compatibility with the propylene copolymer B. The propylene copolymer B, or constituents of the propylene copolymer B, thus act as plasticizer(s) for the matrix. An increase in the comonomer content of the propylene copolymer B results in an improvement in the impact toughness, particularly at low temperatures, but at the expense of the transparency. In addition, the proportion of propylene copolymer B which is miscible with the matrix and acts

as plasticizer is decreased, as a result of which the stiffness of the copolymer increases. At the same time, it is also possible to decrease the stiffness by increasing the proportion of the propylene copolymer B. Accordingly, the products of the present invention display an advantageous combination of these properties, i.e. flexible products which are at the same time transparent are obtained. The transparency of the propylene copolymer compositions of the present invention is virtually independent of the proportion of the propylene copolymer B present therein.

Adjustment of the viscosity ratio of propylene copolymer A to propylene copolymer B influences the dispersion of the propylene copolymer B in the polymer matrix and thus has effects on the transparency of the propylene copolymer compositions and on the mechanical properties.

The propylene copolymer compositions of the present invention display a high flexibility in combination with a good transparency. Furthermore, they have low proportions of n-hexane-soluble material, good stress whitening behavior and also a good impact toughness at low temperatures, a high stiffness and good heat distortion resistance. Since the temperature for the brittle/tough transition is below 0°C, the propylene copolymer compositions of the present invention can also be used in a temperature range which places high demands on the material properties of the copolymers at temperatures below freezing point. A further advantage is that the shrinkage behavior of the propylene copolymer compositions corresponds to that of propylene polymers. In the case of moldings consisting of different materials, for example containers which have been produced from one propylene polymer and are to be closed with a flexible lid, this leads to advantages in respect of accuracy of fit and freedom from leaks, in particular when the containers are subjected to washing at elevated temperatures. This opens up wide-ranging new possibilities for the use of the propylene copolymer compositions of the present invention in transparent applications.

The copolymers of the present invention are suitable for producing fibers, films or moldings, in particular for producing injection-molded parts, films, sheets or large hollow bodies, e.g. by means of injection-molding or extrusion processes. Possible applications are the fields of packaging, household articles, containers for storage and transport, office articles, electrical equipment, toys, laboratory requisites, motor vehicle components and gardening requisites, in each case especially for applications at low temperatures.

The invention is illustrated by the following preferred examples which do not restrict the scope of the invention:

Examples

5

10

15

Preparation of the metallocene catalyst

3 kg of Sylopol 948 were placed in a process filter whose filter plate pointed downward and suspended in 15 l of toluene. 7 l of 30% strength by weight MAO solution (from Albemarle) were metered in while stirring at such a rate that the internal temperature did not exceed 35°C. After stirring for a further 1 hour at a low stirrer speed, the suspension was filtered, firstly with no applied pressure and then under a nitrogen pressure of 3 bar. Parallel to the treatment of the support material, 2.0 1 of 30% strength by weight MAO solution were placed in a reaction vessel, 92.3 g of rac-dimethylsilyl(2-methyl-4-(para-tert-butylphenyl)indenyl)(2isopropyl-4-(para-tert-butylphenyl)indenyl)zirconium dichloride, prepared according to example 18 of WO 01/48034, were added, the solution was stirred for 1 hour and allowed to settle for a further 30 minutes. The solution was subsequently run onto the pretreated support material with the outlet closed. After the addition was complete, the outlet was opened and the filtrate was allowed to run off. The outlet was subsequently closed, the filter cake was stirred for 15 minutes and allowed to stand for 1 hour. The liquid was then pressed out from the filter cake by means of a nitrogen pressure of 3 bar with the outlet open. 151 of isododecane were added to the solid which remained, the mixture was stirred for 15 minutes and filtered. The washing step was repeated and the filter cake was subsequently pressed dry by means of a nitrogen pressure of 3 bar. For use in the polymerization, the total amount of the catalyst was resuspended in 15 l of isododecane.

25

20

30

Polymerization

The process was carried out in two stirring autoclaves which were connected in series and each had a utilizable capacity of 200 l and were equipped with a free-standing helical stirrer. Both

reactors contained an agitated fixed bed of finely divided propylene polymer.

Propylene and ethylene were passed in gaseous form into the first polymerization reactor and polymerized at a mean residence time as shown in Table 1 by means of the metallocene catalyst at a pressure and temperature as shown in Table 1. The amount of metallocene catalyst metered in was such that the amount of polymer transferred from the first polymerization reactor into the second polymerization reactor corresponded, on average, to the amounts shown in Table 1. The metallocene catalyst was metered in together with the Frisch propylene added to regulate the pressure. Triethylaluminum in the form of a 1 molar solution in heptane was likewise metered into the reactor.

The propylene copolymer obtained in the first gas-phase reactor was transferred together with still active catalyst constituents into the second gas-phase reactor. There, the propylene-ethylene copolymer B was polymerized onto it at a total pressure, a temperature and a mean residence time as shown in Table 1. The ethylene concentration in the reaction gas was monitored by gas chromatography. The weight ratio of the propylene copolymer A formed in the first reactor [A(I)] to the propylene copolymer B formed in the second reactor [B(II)] is shown in Table 1. Isopropanol (in the form of a 0.5 molar solution in heptane) was likewise metered into the second reactor. The weight ratio of the polymer formed in the first reactor to that formed in the second reactor was controlled by means of isopropanol which was metered into the second reactor in the form of a 0.5 molar solution in heptane and is shown in Table 1. To regulate the molar mass, hydrogen was metered into the second reactor as necessary. The proportion of propylene-ethylene copolymer B formed in the second reactor is given by the difference of amount transferred and amount discharged according to the relationship (output from second reactor — output from first reactor)/output from second reactor.

Table 1: Polymerization conditions

		Example 1
	Reactor I	
5	Pressure [bar]	28
	Temperature [°C]	73
	Triethylaluminum, 1M in heptane [ml/h]	85
10	Ethylene [% by volume]	3
	Residence time [h]	1.5
	C ₂ [% by weight] in powder (IR)	0.7
	Powder MFR (230°C/2.16 kg) [g/10 min]/ISO 1133	12.9
	Powder output [kg/h]	31
15	Reactor II	
	Pressure [bar]	18.1
	Temperature [°C]	75
	Ethylene [% by volume]	28
20	Residence time [h]	1.1
	Powder output [kg/h]	45
	Powder MFR (230°C/2.16 kg) [g/10 min]/ISO 1133	11
	Content of propylene-ethylene copolymer A [% by	69
25	weight]	
	Content of propylene-ethylene copolymer B [% by	31
	weight]	

*) Standard l/h: standard liters per hour

The polymer powder obtained in the polymerization was admixed with a standard additive mixture in the granulation step. Granulation was carried out using a twin-screw extruder ZSK 30 from Werner & Pfleiderer at a melt temperature of 250°C. The propylene copolymer composition

obtained contained 0.04% by weight of Irganox 1010 (from Ciba Specialty Chemicals), 0.07% by weight of Irgafos 168, (from Ciba Specialty Chemicals), and 0.04% by weight of calcium stearate.

35

The properties of the propylene copolymer composition are shown in Tables 2 and 3. The data were determined on the propylene copolymer composition after addition of additives and granulation or on test specimens produced therefrom.

Table 2: Analytical results on the propylene copolymer composition

		Example 1
5	Proportion of n-hexane-soluble material [% by weight]	1.9
	C ₂ content (IR) [% by weight]	3.5
	C ₂ content of propylene-ethylene copolymer B (IR) [%	9.5
	by weight]	
10	PEP* (IR) [% by weight]	6.3
	PE _x * (IR) [% by weight]	3.0
	Molar mass distribution [M _w /M _n]	2.4

*) The PEP and PE_x values were determined on a propylene-ethylene copolymer which had been separated off from a product which was polymerized under the conditions of Example 1 but without addition of ethylene in the first polymerization step.

Table 3: Use-related tests on the propylene copolymer composition

					Example 1
	MFR	(230°C/2,16	kg)	[g/10 min]/	10
5	ISO 1133				
	DSC melting	g point [°C]/ ISO	3146		145.5
	Brittle/tough	transition tempe	erature [°C]		-6
10					
	Tensile E mo	odulus [MPa]/IS0	O 527		608
	Stress at yiel	d [N/mm²]			21.7
	Elongation a	t yield [%]			16.3
15	Stress at brea	ak [N/mm²]			29.7
	Elongation at break [%]				29.6
	Haze	(1	mm*)	[%]/	34
	ASTM D 10	03			

*) Injection-molded plates having a thickness of 1 mm.

Analysis

20

25

30

35

The production of the test specimens required for the use-related tests and the tests themselves were carried out in accordance with the standards indicated in Table 3.

The proportion of n-hexane-soluble material was determined by extraction using a modified FDA method. About 2.5 g of granules were weighed out and suspended in 1 l of n-hexane. The suspension was heated to $50^{\circ}\text{C} \pm 0.2^{\circ}\text{C}$ over a period of 20-25 minutes while stirring and stirred for a further 2 hours at this temperature. The suspension was filtered through a glass frit which had been preheated to 50°C . About 350 g of the filtrate were weighed into an evaporator flask which had previously been dried over P_2O_5 in a desiccator for 12 hours. The filtrate was evaporated to about 20-30 ml at 60°C under reduced pressure on a rotary evaporator. The solution was transferred quantitatively with the aid of several rinses with warm hexane into a 200 ml evaporating basin which had previously been dried over P_2O_5 in a desiccator for 12 hours and weighed. The solution was evaporated to dryness on a hotplate while passing nitrogen over it. After evaporation, the evaporating basin was dried over P_2O_5 at 200 mbar in a desiccator for 12 hours, weighed and the extraction residue was determined. The same procedure was repeated without addition of polymer granules and the residue in

pure n-hexane was determined. The residue in pure n-hexane was subtracted to determine the proportion of material which is extracted by n-hexane.

The brittle/tough transition was determined by means of the puncture test described in ISO 6603-2/40/20/C/4.4. The velocity of the punch was chosen as 4.4 m/s, the diameter of the support ring was 40 mm and the diameter of the impact ring was 20 mm. The test specimen was clamped in. The test specimen geometry was 6 cm × 6 cm at a thickness of 2 mm. To determine the temperature dependence curve, measurements were carried out at steps of 2°C in the temperature range from 26°C to -35°C using a test specimen preheated/precooled to the respective temperature.

In the present example, the brittle/tough transition was determined from the total deformation in mm defined as the displacement through which the punch has traveled when the force has passed through a maximum and dropped to 3% of this maximum force. For the purposes of the present invention, the brittle/tough transition temperature is defined as the temperature at which the total deformation is at least 25% below the mean total deformation of the preceding 5 measurement points.

The determination of the Haze values was carried out in accordance with the standard ASTM D 1003. The test specimens were injection-molded plates having an edge length of 6 x 6 cm and a thickness of 1 mm. The test specimens were injection molded at a melt temperature of 250°C and a tool surface temperature of 30°C. After a storage time of 7 days at room temperature for after-crystallization, the test specimens were clamped into the clamping device in front of the inlet orifice of a Hazegard System XL 211 from Pacific Scientific and the measurement was subsequently carried out. Testing was carried out at 23°C, with each test specimen being examined once in the middle. To obtain a mean, 5 test specimens were tested in each case.

The stress whitening behavior was assessed by means of the domed method. In the dome method, the stress whitening was determined by means of a falling dart apparatus as specified in DIN 53443 Part 1 using a falling dart having a mass of 250 g, a punch diameter of 5 mm and a dome radius of 25 mm. The drop was 50 cm. As test specimen, use was made of an injection-molded circular disk having a diameter of 60 mm and a thickness of 2 mm. The test specimen was injection molded at a melt temperature of 250°C and a tool surface temperature of 30°C. Testing was carried out at 23°C, with each test specimen being subjected to only one impact test. The test specimen was first laid on a support ring without being clamped and the

falling dart was subsequently released. To obtain the mean, at least five test specimens were tested. The diameter of the visible stress whitening region is reported in mm and was determined by measuring this region in the flow direction and perpendicular thereto on the side of the circular disk opposite that on which impact occurs and forming the mean of the two values.

The C₂ content of the propylene-ethylene copolymers was determined by means of IR spectroscopy.

The structure of the propylene-ethylene copolymer B was determined by means of ¹³C-NMR spectroscopy.

The tensile E modulus was measured in accordance with ISO 527-2:1993. The test specimen of type 1 having a total length of 150 mm and a parallel section of 80 mm was injection molded at a melt temperature of 250°C and a tool surface temperature of 30°C. To allow after-crystallization to occur, the test specimen was stored for 7 days under standard conditions of 23°C/50% atmospheric humidity. A test unit model Z022 from Zwick-Roell was used for testing. The displacement measurement system in the determination of the E modulus had a resolution of 1 μ m. The testing velocity in the determination of the E modulus was 1 mm/min, otherwise 50 mm/min. The yield point in the determination of the E modulus was in the range 0.05%-0.25%.

The determination of the melting point was carried out by means of DSC (differential scanning calorimetry). The measurement was carried out in accordance with ISO standard 3146 using a first heating step at a heating rate of 20°C per minute up to 200°C, a dynamic crystallization at a cooled rate of 20°C per minute down to 25°C and a second heating step at a heating rate of 20°C per minute back up to 200°C. The melting point is then the temperature at which the enthalpy versus temperature curve measured during the second heating step displays a maximum.

The determination of the molar mass M_n and the molar mass distribution M_w/M_n was carried out by gel permeation chromatography (GPC) at 145°C in 1,2,4–trichlorobenzene using a GPC apparatus model 150C from Waters. The data were evaluated by means of the Win-GPC software from HS–Entwicklungsgesellschaft für wissenschaftliche Hard– und Software mbH, Ober–Hilbersheim. The columns were calibrated by means of polypropylene standards having molar masses from 100 to 10^7 g/mol.

5

10

15

20

25

30

Claims

5

10

25

30

40

- 1. A propylene copolymer composition comprising
 - A) from 50% to 80% by weight of a propylene copolymer containing from 0.05 to 0.99% by weight of an alpha olefins having from 2 to 10 carbon atoms other than propylene; and
 - B) from 20% to 50% by weight of one propylene copolymer containing from 7.01 to 9.99 % by weight of an alpha olefins having from 2 to 10 carbon atoms other than propylene;

said propylene copolymer composition having the following characteristics:

- (i) MFR (230°C/2,16 kg) comprised between 6 and 12 g/10 min;
- (ii) tensile E modulus comprised between 550 and 750 MPa (ISO 527-2:1993).
- 2. The propylene copolymer composition as claimed in claim 1 having a melting point comprised between 143°C and 150°C.
 - 3. The propylene copolymer composition as claimed in claims 1-2 having haze (ASTM D 1003) comprised between 25% and 40% without the adding of clarifying agents.
- 4. A propylene copolymer composition as claimed in claim 1, wherein the catalyst system comprises at least one metallocene compound of the formula (I),

35 where

- M is zirconium, hafnium or titanium,
- X are identical or different and are each, independently of one another, hydrogen or halogen or an -R, -OR, -OSO₂CF₃, -OCOR, -SR, -NR₂ or -PR₂ group, where R is linear or branched C₁-C₂₀-alkyl, C₃-C₂₀-cycloalkyl which may be

substituted by one or more C1-C10-alkyl radicals, C6-C20-aryl, C7-C20-alkylaryl or C7-C20-arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the Elements or one or more unsaturated bonds, where the two radicals X may also be joined to one another, 5 is a divalent bridging group selected from the group consisting of C1-C20- \mathbf{L} alkylidene radicals, C₃-C₂₀-cycloalkylidene radicals, C₆-C₂₀-arylidene radicals, C7-C20-alkylarylidene radicals and C7-C20-arylalkylidene radicals, which may contain heteroatoms of groups 13-17 of the Periodic Table of the Elements, or 10 a silylidene group having up to 5 silicon atoms, e.g. -SiMe₂- or -SiPh₂-, is linear or branched C1-C20-alkyl, C3-C20-cycloalkyl which may be substituted \mathbb{R}^1 by one or more C₁-C₁₀-alkyl radicals, C₆-C₂₀-aryl, C₇-C₂₀-alkylaryl or C₇-C₂₀arylalkyl and may contain one or more heteroatoms of groups 13-17 of the 15 Periodic Table of the Elements or one or more unsaturated bonds, where R1 is preferably a linear or branched C1-C10-alkyl group which is unbranched in the a position, in particular a linear C1-C4-alkyl group such as methyl, ethyl, n-propyl or n-butyl, is a group of the formula -C(R³)₂R⁴, where 20 \mathbb{R}^2 are identical or different and are each, independently of one another, linear or \mathbb{R}^3 branched C1-C20-alkyl, C3-C20-cycloalkyl which may be substituted by one or more C_1 - C_{10} -alkyl radicals, C_6 - C_{20} -aryl, C_7 - C_{20} -alkylaryl or C_7 - C_{20} -arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic 25 Table of the Elements or one or more unsaturated bonds, or two radicals R³ may be joined to form a saturated or unsaturated C3-C20-ring, is hydrogen or linear or branched C1-C20-alkyl, C3-C20-cycloalkyl which may R^4 be substituted by one or more C₁-C₁₀-alkyl radicals, C₆-C₂₀-aryl, C₇-C₂₀-30 alkylaryl or C7-C20-arylalkyl and may contain one or more heteroatoms of

T and T' are divalent groups of the formulae (II), (III), (IV), (V) or (VI),

groups 13-17 of the Periodic Table of the Elements or one or more unsaturated

35

bonds,

20

25

35

40

15

5

10

where

the atoms denoted by the symbols * and ** are joined to the atoms of the compound of the formula (I) which are denoted by the same symbol, and

(VI)

 \mathbb{R}^5 30

(V)

are identical or different and are each, independently of one another, hydrogen or halogen or linear or branched C1-C20-alkyl, C3-C20-cycloalkyl which may be substituted by one or more C_1 - C_{10} -alkyl radicals, C_6 - C_{20} -aryl, C_7 - C_{20} -alkylaryl or C_7 - C_{20} -arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the Elements or one or more unsaturated bonds,

 \mathbb{R}^6

are identical or different and are each, independently of one another, halogen or a linear or branched C1-C20-alkyl, C3-C20-cycloalkyl which may be substituted by one or more C₁-C₁₀-alkyl radicals, C₆-C₂₀-aryl, C₇-C₂₀-alkylaryl or C₇-C₂₀arylalkyl and may contain one or more heteroatoms of groups 13-17 of the Periodic Table of the Elements or one or more unsaturated bonds.

A propylene copolymer composition as claimed in any of claims 1 to 4, wherein the 5. olefin other than propylene is exclusively ethylene.

- 6. A propylene copolymer composition as claimed in any of claims 1 to 5, wherein the molar mass distribution M_w/M_n is in the range from 1.5 to 3.5.
- 7. The use of a propylene copolymer composition as claimed in any of claims 1 to 6 for producing fibers, films or moldings.

Abstract

A propylene copolymer composition comprising

- A) from 50% to 80% by weight of a propylene copolymer containing from 0.05 to 0.99% by weight of an alpha olefins having from 2 to 10 carbon atoms other than propylene; and
- B) from 20% to 50% by weight of one propylene copolymer containing from 7.01 to 9.99 % by weight of an alpha olefins having from 2 to 10 carbon atoms other than propylene;

said propylene copolymer composition having the following characteristics:

- (i) MFR (230°C/2,16 kg) [g/10 min] comprised between 6 and 12;
- (ii) tensile E modulus comprised between 550 and 750 MPa (ISO 527-2:1993).

15

5

10

20

25

30

•· • • • • • • • • • • • • • • • • • •	
	ž., .
	: